

Coupled formulations and coupling algorithms for reactive transport in porous media

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- 1 Motivations
- 2 Basic models and methods
 - Flow model
 - Transport model
 - Chemistry
- 3 Formulations and solution methods
 - Reactive transport
 - Algorithms
- 4 Examples
 - Ion exchange
 - CO2 example
- 5 Conclusions

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Nuclear waste storage (1)

- Assess safety of deep geological nuclear waste storage (clay layer)
- Long term simulation of radionuclide transport (one million years)
- Wide variation of scales : from package (meter) to regional (kilometers)
- Geochemistry : large number of species
- Strong government regulation



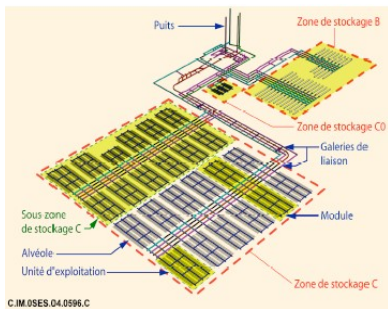
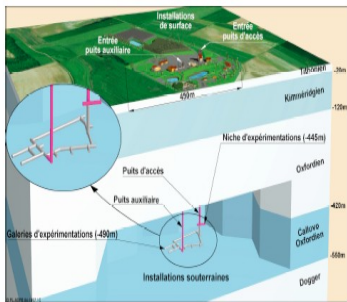
● Main actors : **ANDRA**,



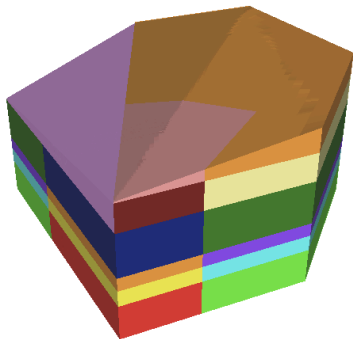
- Research in mathematical and numerical modeling is conducted in the CNRS **MOMAS** group (Director A. Ern).

Nuclear waste storage (2)

Present choice in France : a **sedimentary** geological formation (Bures, in the Meuse region)



A 3D far field model (V. Martin)

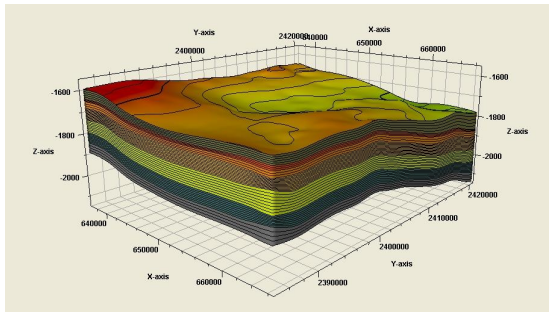


Blown-up 30 times vertically

Difficulties

- Distorted geometry (horizontal \approx 40 km, vertical 700 m)
- Strong heterogeneities (permeability varies by 8 orders of magnitude)
- General hexahedral mesh
- Simulation over 500 000 years

CO₂ sequestration



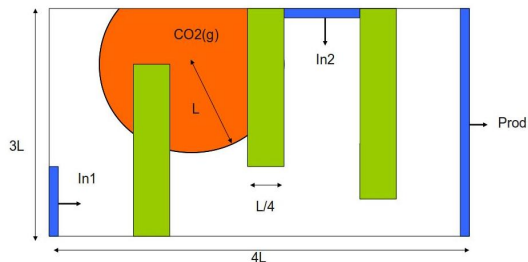
Geological model, BRGM (21 million grid points)

- Long term capture of CO₂ in saline aquifer
- Simulation to understand CO₂ migration through salt
- Coupling of liquid and gas phase, reactive transport

ANR SHPCO2 project High Performance Simulation of CO₂ sequestration

CO₂ sequestration : a synthetic model

Minimal chemical system that still "looks" realistic for CO₂ storage



Dissolution of CO₂ in water, dissolution of calcite. Gas assumed **immobile** (capillary trapping), decouples flow from reactive transport.

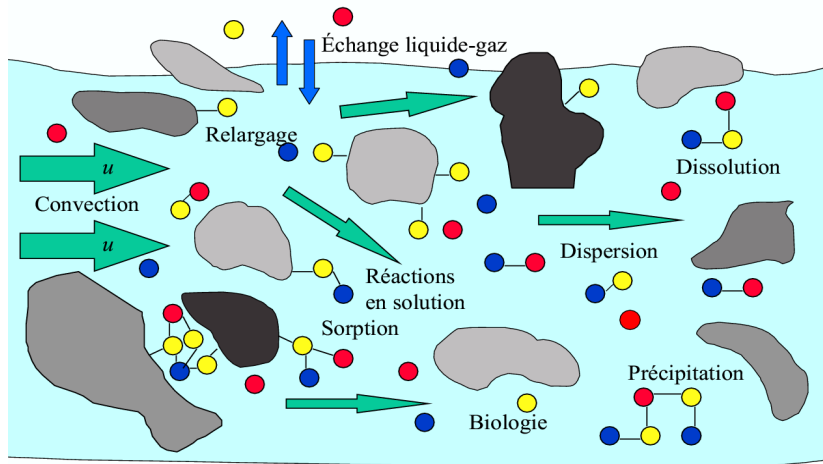
Chemical system

- $\text{H}_2\text{O} \rightleftharpoons \text{H}^+ + \text{OH}^-$ water dissociation
- $\text{CO}_2(\text{g}) \rightleftharpoons \text{CO}_2(\text{aq})$ gas dissolution
- $\text{H}_2\text{O} + \text{CO}_2(\text{aq}) \rightleftharpoons \text{HCO}_3^- + \text{H}^+$ dissociation of aqueous CO₂
- $\text{CaCO}_3 + \text{H}^+ \rightleftharpoons \text{Ca}_2^+ + \text{HCO}_3^-$ Dissolution of calcite

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Transport and chemical phenomena



Flow model

Flow equations

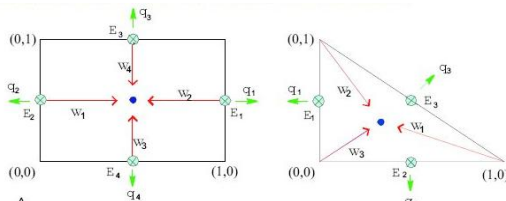
$$\mathbf{q} = -K \nabla h \quad \text{Darcy's law} \quad h \text{ piezometric head}$$

$$\nabla \cdot \mathbf{q} = 0 \quad \text{incompressibility} \quad \mathbf{q} \text{ Darcy velocity}$$

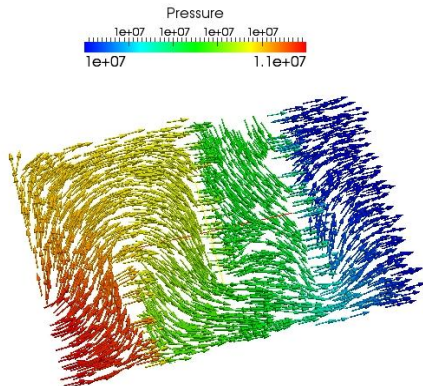
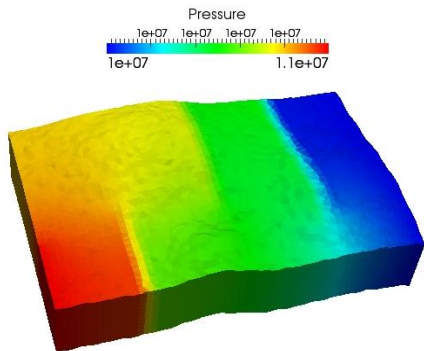
K permeability tensor (heterogeneous, anisotropic)

Mixed finite elements

- Approximate both **head** and **velocity**
- Locally **mass conservative**
- Continuous **flux** across element faces
- Allows **full** diffusion tensor



Pressure and velocity for CO2 example (A. Fumagalli, M. Franco)



Transport model

Convection–diffusion equation

$$\phi \frac{\partial c}{\partial t} - \underbrace{\operatorname{div}(\mathbf{D} \operatorname{grad} c)}_{\text{dispersion}} + \underbrace{\operatorname{div}(\mathbf{q}c)}_{\text{advection}} + \phi \lambda c = f$$

- c : concentration [mol/l]
- ϕ : porosity [–]
- λ radioactive decay [s^{-1}]
- \mathbf{q} Darcy velocity [m/s]

Dispersion tensor

$$\mathbf{D} = d_e \mathbf{I} + |\mathbf{q}| [\alpha_l \mathbf{E}(\mathbf{q}) + \alpha_t (I - \mathbf{E}(\mathbf{q}))], \quad E_{ij}(\mathbf{q}) = \frac{q_i q_j}{|\mathbf{q}|}$$

α_l, α_t dispersivity coeff. [m], d_e molecular diffusion [m^2/s]

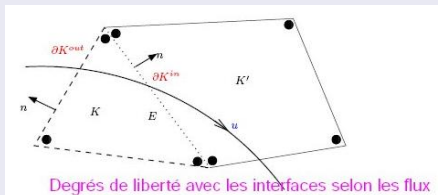
Notation $\operatorname{div}(\mathbf{q}c - \mathbf{D} \operatorname{grad} c) + \phi \lambda c \stackrel{\text{def}}{=} Lc$

Solution by operator splitting

Advection step

Explicit, finite volumes / discontinuous Galerkin

- Locally mass **conservative**
- Allows **unstructured** mesh
- CFL condition : use **sub-time-steps**



Dispersion step

Like flow equation (time dependent) : mixed finite elements (implicit)

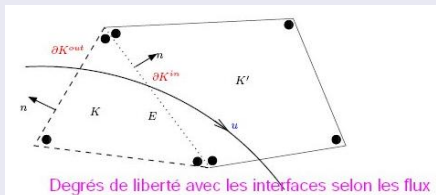
See Ackerer et al., Putti et al., Arbogast et al., ...

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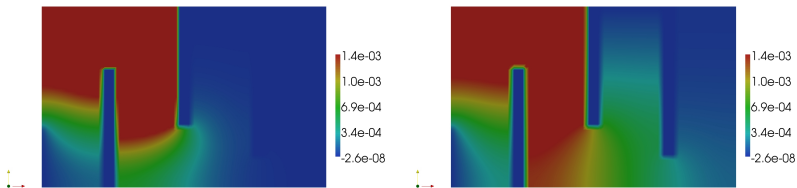
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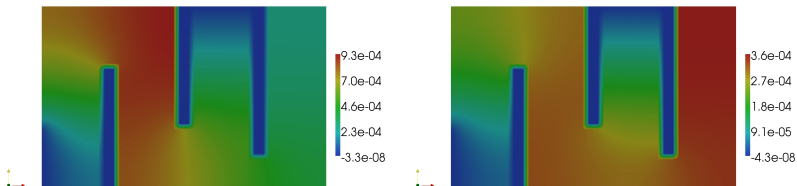
Condense transport solver, one time step

$$C^{n+1} = \Psi_T(f^n, C^n)$$

Transport for synthetic CO₂ example



Left $T = 1$ day, right $T = 6$ days



Left $T = 12$ day, right $T = 37$ days

Classification of chemical reactions

According to nature of reaction

Homogeneous In the same phase (aqueous, gaseous, ...)

Examples : Acid base, oxydo–reduction

Heterogeneous Involve different phases

Examples : Sorption, mineral precipitation / dissolution, gas dissolution, ...

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Slow reactions Irreversible, modeled using kinetic law

Fast reactions Reversible, modeled using equilibrium

Depends on relative speed of reactions and transport.

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This talk : only **equilibrium** reactions

Sorption processes

Definition

Sorption is the accumulation of a fluid on a solid at the fluid–solid interface.

Main mechanism for exchanges between dissolved species and solid surfaces.

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Ion exchange Ions are exchanged between sorption **sites** on the surface. Depends on **Cationic Exchange Capacity**.

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Can be modeled as **mass action law**

Modeling general equilibrium models

General chemical reactions : N_s species, N_r reactions

$$\sum_{j=1}^{N_s} v_{ij} Y_j \rightleftharpoons 0, \quad i = 1, \dots, N_r$$

v_{ij} **stoichiometric** coefficients. Matrix equation $vY = 0$

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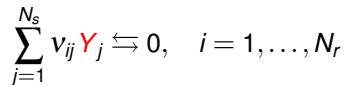
Basis for null-space of v has dimensions $N_c = N_s - N_r$.

Partition $v = (G \ N)$, $B \in \mathbf{R}^{N_r \times N_r}$ invertible, $N \in \mathbf{R}^{N_c \times N_r}$. Let $H = -G^{-1}N$

General solution of $vY = 0$: $Y = \begin{pmatrix} x \\ c \end{pmatrix}$, $x = Hc$. $c \in \mathbf{R}^{N_c}$, $x \in \mathbf{R}^{N_r}$.

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Morel formalism :

(c, \bar{c}) primary species	(x, \bar{x}) secondary species
(c, x) mobile species	(\bar{c}, \bar{x}) fixed species

Chemical equilibrium (aqueous and sorption reactions)

Chemical reactions, mass action laws

$$x_i \rightleftharpoons \sum_{j=1}^{N_c} S_{ij} c_j, \quad i = 1, \dots, N_x,$$

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System of non-linear equations

Mass action law

$$\log x = S \log c + \log K,$$

$$\log \bar{x} = A \log c + B \log \bar{c} + \log \bar{K}.$$

Mass conservation

$$c + S^T x + A^T \bar{x} = T, \quad T \text{ known from transport}$$

$$\bar{c} + B^T \bar{x} = W, \quad W \text{ imposed}$$

Mineral reactions

Dissolution of solid, precipitation of aqueous species. Reactions with threshold : **which** species appear unknown a priori.

Solubility product $\Pi = \log K_p + S_p \log c$

$$\begin{cases} p = 0 & \text{if } \Pi < 0 \\ \Pi = 0 & \text{otherwise} \end{cases}$$

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Solution methods

- Standard procedure : **combinatorial** search
- Reformulate as **complementarity** problem
- **Interior point** algorithm (Saaf et al. ('96), MK (05))
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Remark

Same treatment for gas, with **Henry's** law

Numerical solution of nonlinear problem

Take concentration **logarithms** as main unknowns

Use **globalized** Newton's method (line search, trust region).

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Role of chemical model

Given totals T (and W , known), split into

$$\text{Mobile } C = c + S^T x,$$

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Result of chemical problem

$$F = \Psi_C(T)$$

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Reactive transport model

Balance equations

$$\begin{aligned}\phi \partial_t \mathbf{c} + \mathbf{Lc} &= \mathbf{S}_{mm}^T \mathbf{R}_e^a + \mathbf{S}_{mf}^T \mathbf{R}_e^h \\ \phi \partial_t \bar{\mathbf{c}} &= \mathbf{S}_{ff}^T \mathbf{R}_e^h\end{aligned}$$

R_e equilibrium rates **unknown**,

Reactive transport model

Balance equations

$$\begin{aligned}\phi \partial_t \mathbf{c} + L\mathbf{c} &= S_{mm}^T R_e^a + S_{mf}^T R_e^h \\ \phi \partial_t \bar{\mathbf{c}} &= S_{ff}^T R_e^h\end{aligned}$$

R_e equilibrium rates **unknown**,

Elimination of equilibrium rates

$$\begin{aligned}\phi \frac{\partial T^{ic}}{\partial t} + L(C^{ic}) &= 0, \quad ic = 1, \dots, N_c \\ T_{ix}^{ic} &= C_{ix}^{ic} + F_{ix}^{ic} \quad ic = 1, \dots, N_c \text{ and } ix = 1, \dots, N_x \\ F_{ix} &= \Psi_C(T_{ix}) \quad ix = 1, \dots, N_x.\end{aligned}$$

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Fixed point (aka OS) Yeh–Tripathi, Carrayrou et al., Carrera et al.

- + easy to program, code reuse
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DAE formulation Erhel and de Dieuleveult

- + use quality DAE software, accurate
- – expensive

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Elimination technique Knabner et al.

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- – difficult to code

A global method from the fixed–point formulation (1)

Discrete non-linear system

$$\begin{cases} C^{n+1} = \Psi_T \left(\phi \frac{F^n - F^{n+1}}{\Delta t}, C^n \right) \\ F^{n+1} = \Psi_C(C^{n+1} + F^{n+1}) \end{cases}$$

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Can be solved by block Gauss Seidel or by **Newton's** method

A global method from the fixed–point formulation (2)

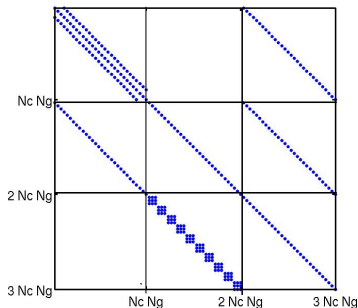
- + **Non-intrusive** approach
- + **Precipitation** can be included
- – One chemical equilibrium **solve** for each function evaluation

A global method from the fixed–point formulation (2)

- + **Non-intrusive** approach
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- – One chemical equilibrium **solve** for each function evaluation

Solution by **Newton–Krylov** method

- Solve the linear system by an **iterative** method (GMRES)
- Requires only jacobian matrix by vector products, Jacobian not stored
- Keep transport and chemistry as black–boxes (up to Jacobian computation)

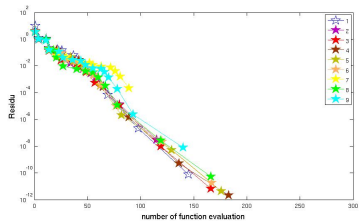
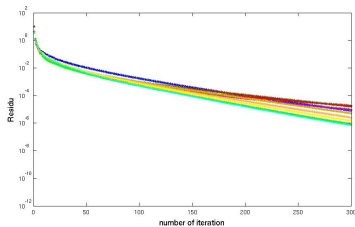


Jacobian structure

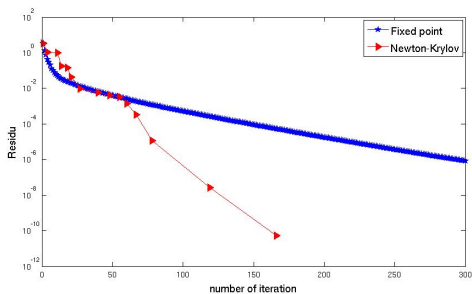
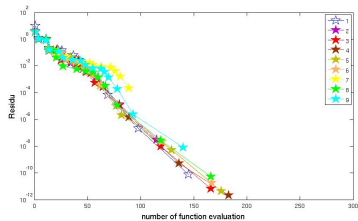
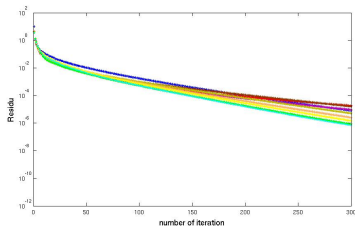
Newton–Krylov method

Used for CFD, shallow water, radiative transfer (Keyes, Knoll, JCP 04), and for reactive transport (Hammond, Valocchi, Lichtner, Adv. Wat. Res. 05)

Newton vs fixed-point performance



Newton vs fixed-point performance

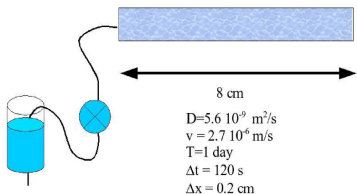


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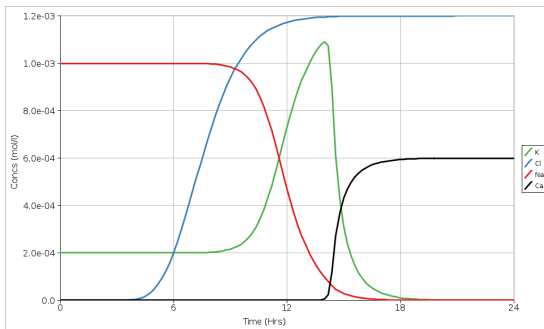
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Example : ion exchange

Column experiment (Phreeqc ex. 11)

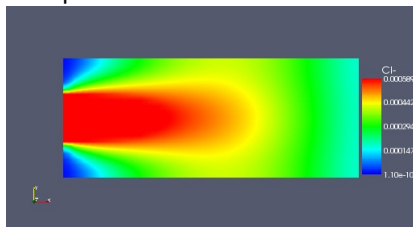


Column contains a solution with 1mmol Na, 0.2mmol K and 1.2mmol NO_3^- . Inject solution with 1.2mmol CaCl_2 , $CEC = 1.1 \cdot 10^{-3}$.

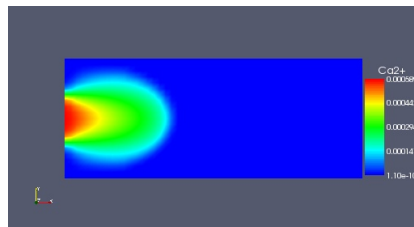


Ion exchange example (ctd)

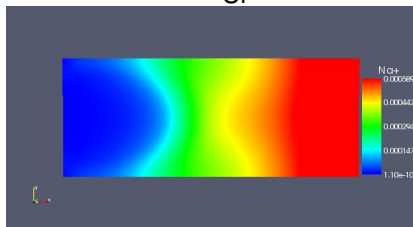
Snapshots at $t = 35$



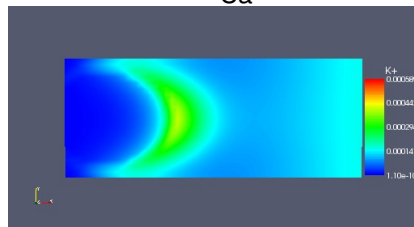
Cl



Ca



Na



K

Application to CO2 model

Simulation code LifeV (EPFL, MOX, INRIA), nonlinear solver Kinsol (LLNL).

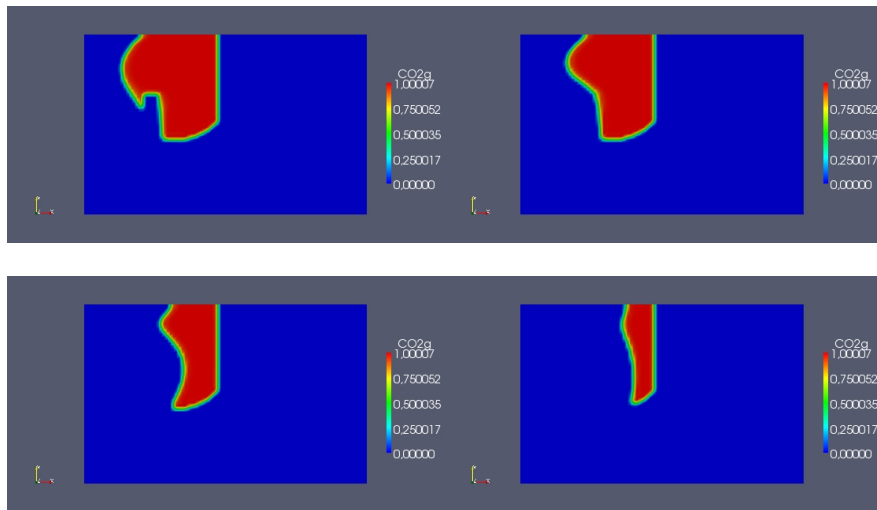
Coarse grid

- 5700 grid points, $\Delta x = 50\text{m}$, $\Delta t = 100$ years
- Simulate 10 000 years
- CPU time 2h10 min

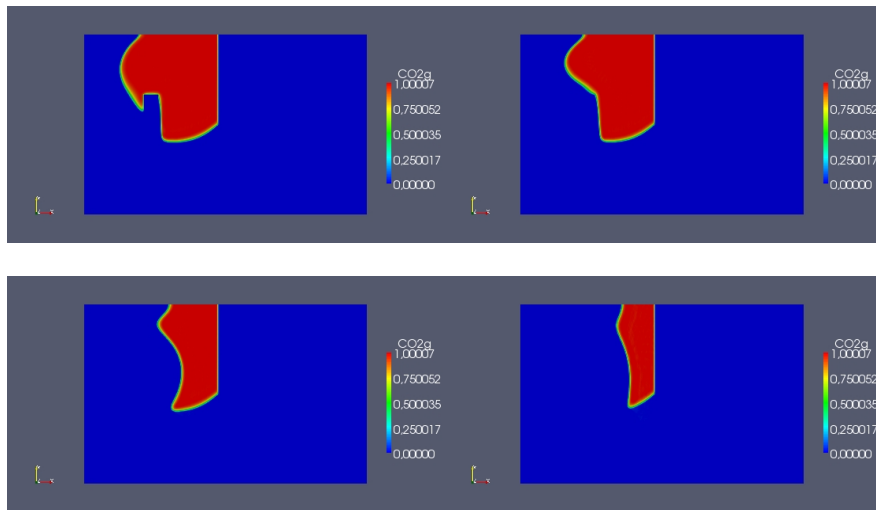
Fine grid

- 142 500 grid points, $\Delta x = 10\text{m}$, $\Delta t = 100$ years
- Simulate 1 600 years
- CPU time 2.5 days

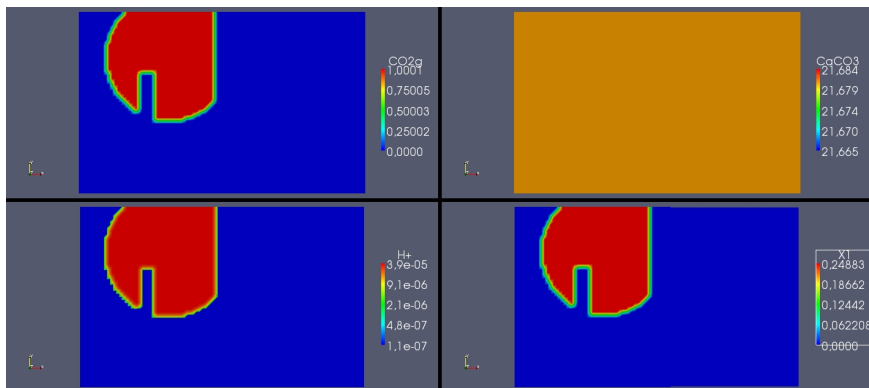
Evolution of CO2 concentration on coarse grid



Evolution of CO2 concentration on fine grid

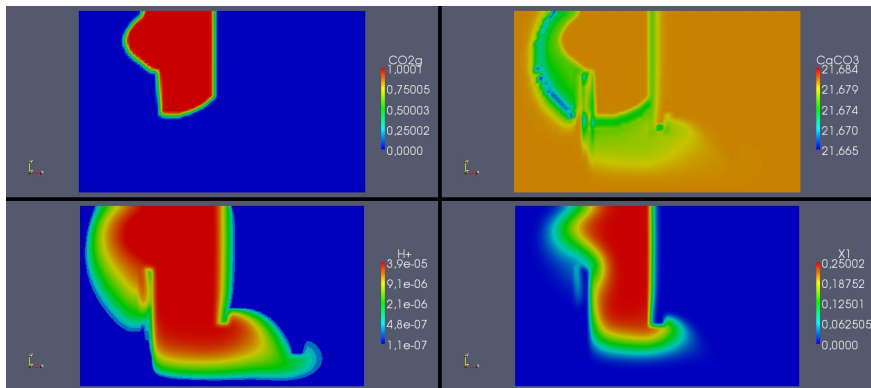


Evolution of concentrations



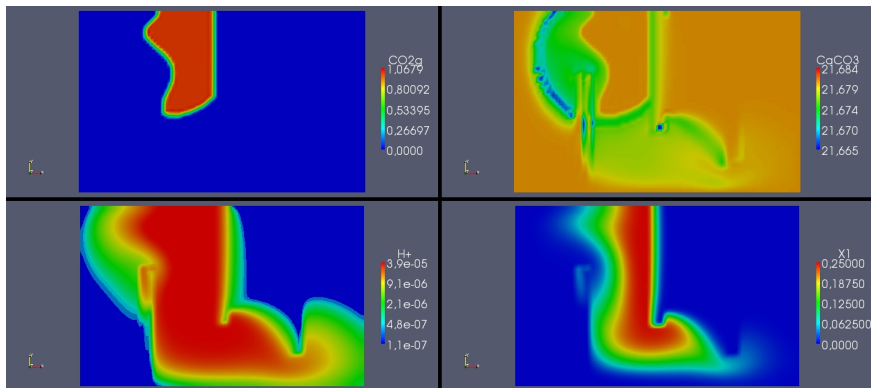
$t = 0$

Evolution of concentrations



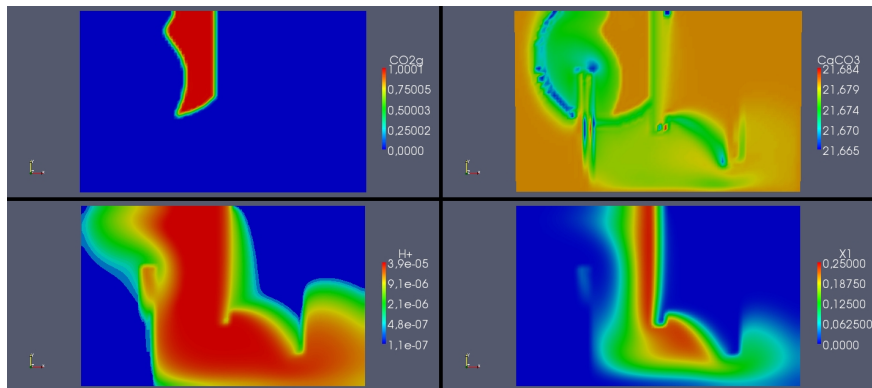
$t = 400$ years

Evolution of concentrations



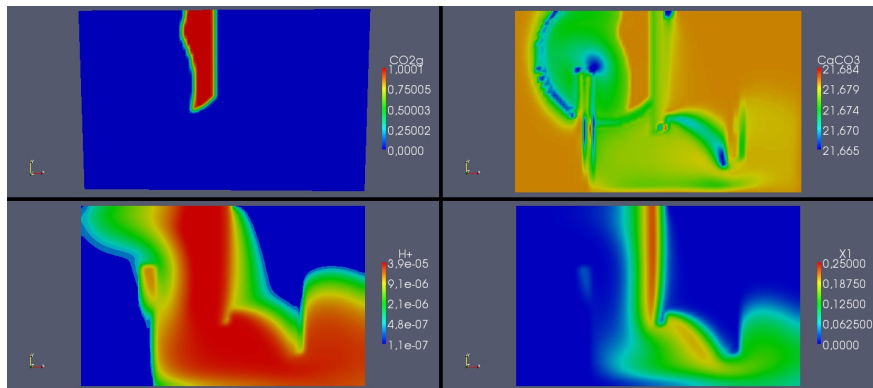
$t = 800$ years

Evolution of concentrations



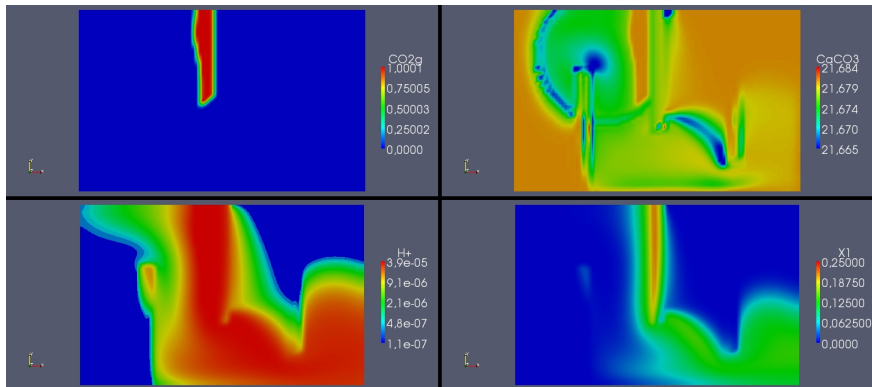
$t = 1200$ years

Evolution of concentrations



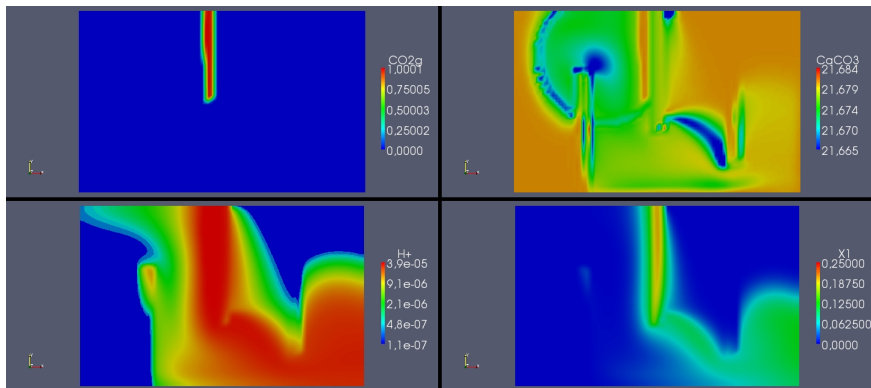
$t = 1600$ years

Evolution of concentrations



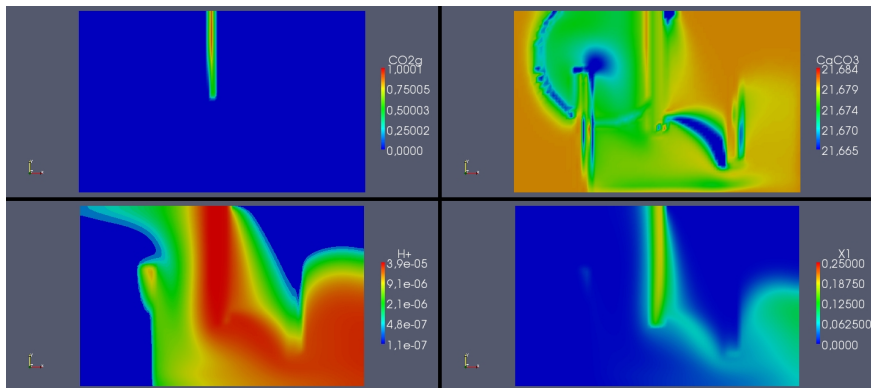
$t = 2000$ years

Evolution of concentrations



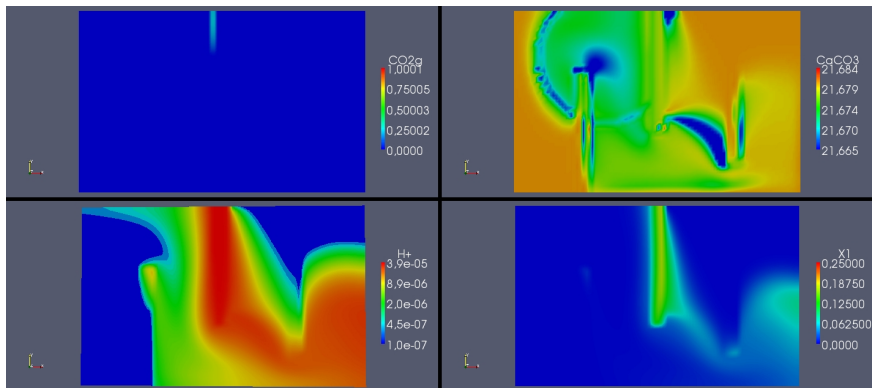
$t = 2400$ years

Evolution of concentrations



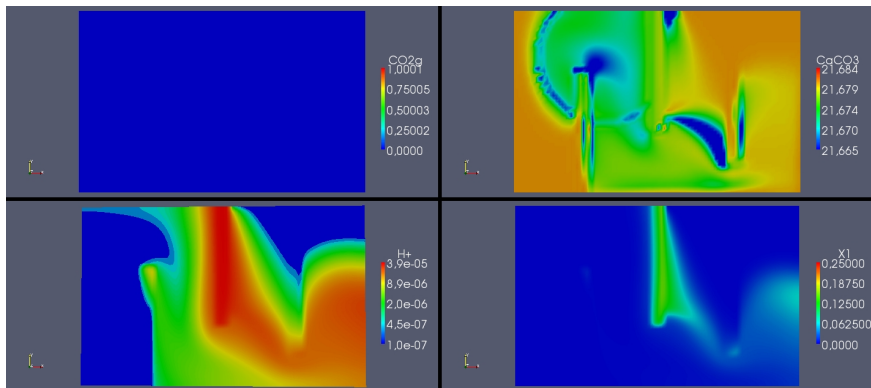
$t = 2800$ years

Evolution of concentrations



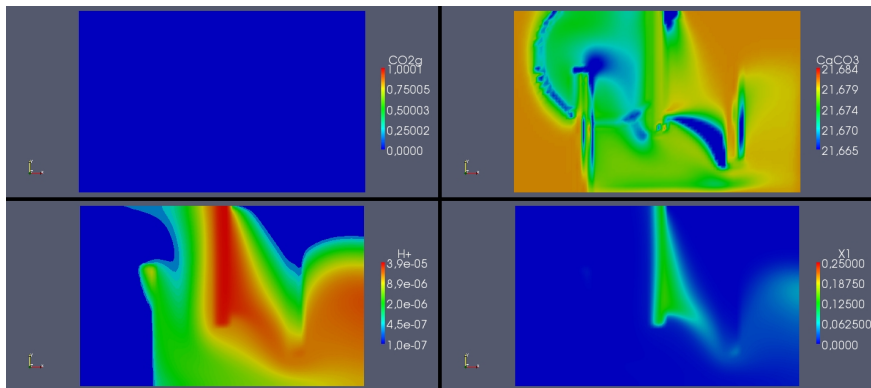
$t = 3200$ years

Evolution of concentrations



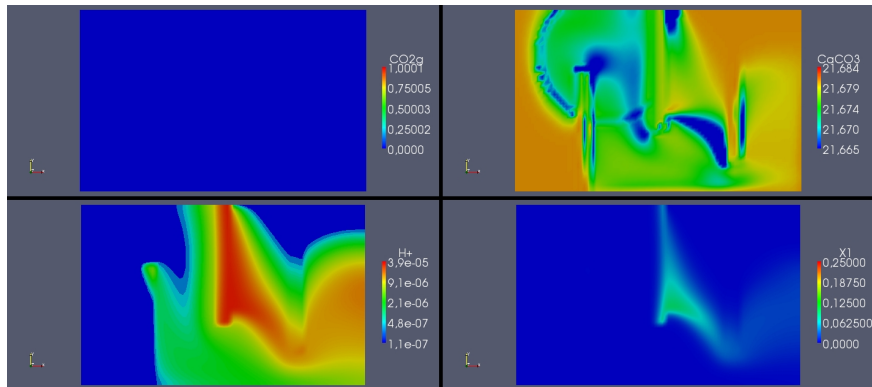
$t = 3600$ years

Evolution of concentrations



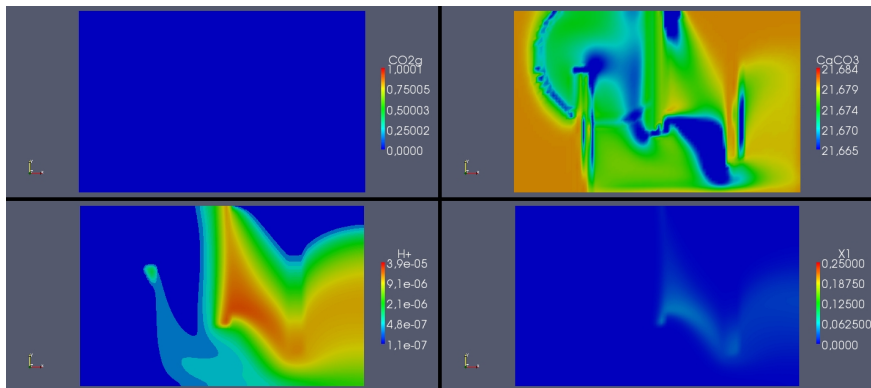
$t = 4000$ years

Evolution of concentrations



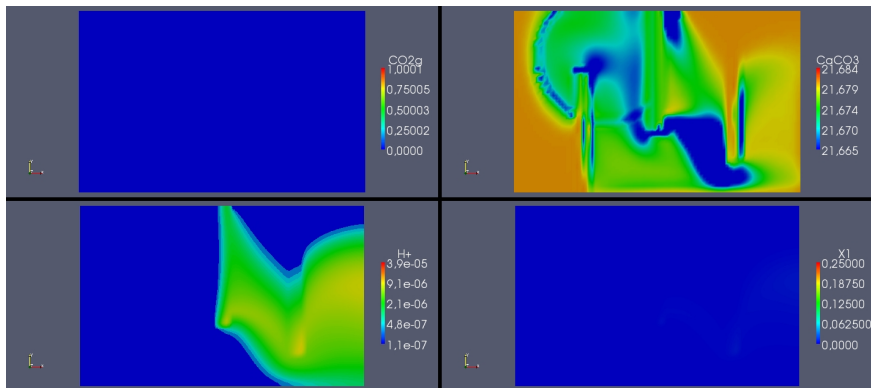
$t = 5000$ years

Evolution of concentrations



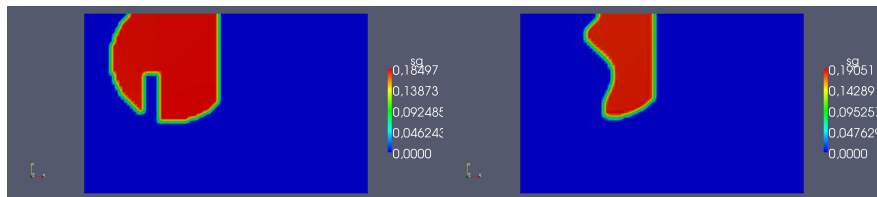
$t = 7000$ years

Evolution of concentrations



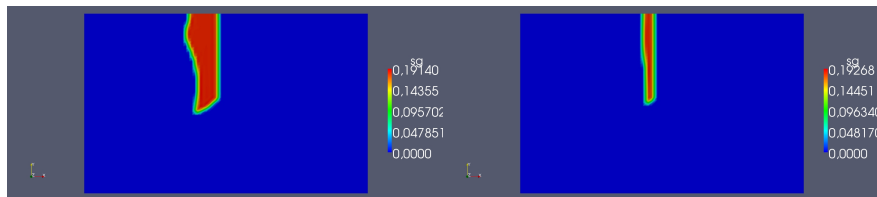
$t = 10000$ years

Evolution of gas saturation



$t = 0$

$t = 800$ years



$t = 1600$

$t = 2400$ years

Outline

- 1 Motivations
- 2 Basic models and methods
 - Flow model
 - Transport model
 - Chemistry
- 3 Formulations and solution methods
 - Reactive transport
 - Algorithms
- 4 Examples
 - Ion exchange
 - CO2 example
- 5 Conclusions

Conclusions – perspectives

- **Robust** methods for flow and transport
- **Newton–Krylov as a framework for code coupling**
- Extension of chemical solver to handle **minerals** and gas
- Preconditioner for simplified system, **mesh independent** convergence

Conclusions – perspectives

- **Robust** methods for flow and transport
- **Newton–Krylov as a framework for code coupling**
- Extension of chemical solver to handle **minerals** and gas
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- Implement **analytical** Jacobian – vector product
- Implement **kinetic** reactions
- **Parallel** computing (w. MOX, Milano)
- Extension to **multiphase** (compositional) flow